# Universität Rostock



Traditio et Innovatio



# Recycling of Phosphorous-based Organocatalysts by Organic Solvent Nanofiltration

J. Großeheilmann<sup>a</sup>, H. Büttner<sup>b</sup>, C. Kohrt<sup>b</sup>, T. Werner<sup>b</sup>, U. Kragl<sup>a,b</sup>

### Introduction

phosphorous-based organocatalysts which Several significantly accelerate the coupling of epoxides and  $CO_2$  with a highly atom efficient reaction under mild conditions were developed.<sup>[1]</sup> The produced cyclic carbonates are versatile organic compounds for the synthesis of organic building blocks, alternative solvents and polymer monomers. However, the separation of the organocatalysts for a subsequent recycling is typically challenging. Herein we evaluate Organic Solvent Nanofiltration (OSN) as promising alternative providing high purities and a low energydemanding separation process.<sup>[2]</sup>



$$Et \longrightarrow 0 + 0 = C = 0 \qquad \frac{5 \text{ mol}\% \left[H0 \longrightarrow PBu_3\right]I}{60 \text{ °C}, 8 \text{ h}, p(CO_2) = 1.0 \text{ MPa}} \qquad \underbrace{0 \longrightarrow 0}_{Et}$$

Scheme 1. Phosphorous-based organocatalyzed synthesis of butylene carbonate.





Figure 1. Scheme of the working process, used in this study.

### Results

# Instrumental Setup **Fresh solvent** Pressure

#### **Filtration Experiments**

Screening experiments with different membranes from DM series (Evonik MET Ltd., UK) were performed. The P-catalyst was rejected with 95.4% (DM 300) and 99.1% (DM 150) respectively, which facilitates a highly selective separation of the catalyst from the product. For recycling experiments EtOH was chosen as solvent because of the highest flux  $(12.7 \text{ Lm}^{-2} \text{ h}^{-1})$  with the membrane DM 300.







Figure 2. Process scheme for the reaction / diafiltration cycle in the cross flow cell: (step 1) reaction of butylene oxide with carbon dioxide to butylene carbonate; (step 2) discontinuous diafiltration of the diluted postreaction mixture (first batch from reaction vessel); (step 2a) repeated filtration; (step 2b) repeated dilution; (step 3) addition of fresh substrates.

Figure 3. Filtration results with different membranes (left). Conditions: 0.15 M P-catalyst in EtOH, 30 bar,  $\vartheta = 25$  °C, stirred cell, n = 2. Filtration results with different solvents (right). Conditions: DM 300, 20 bar,  $\vartheta = 25$  °C, cross flow cell, 70 mL min<sup>-1</sup>, 0.15 M P-catalyst in solvent, n = 2, NM = nitromethane.

#### **Catalyst and Product Separation from Postreaction Mixture**

The reaction mixture consisting of butylene oxide (0.133 mol), P-catalyst 1.0 -Batch III Batch II **Batch I** (5 mol%) and 1.0 MPa carbon dioxide was allowed to react for 8 h at 0.8-60 °C. Conversion and yield were determined prior dilution to 40 mL with EtOH (batch I (Figure 4)). Up to eleven diafiltration steps were performed  $\pm$  0.6 and the feed solution was concentrated to an initial volume of 20 mL to flush out the product. Figure 4 presents the amount of product during the 0.4 reaction / filtration cycle (green points represent the experimental data, white points represent the theoretical data). The product was rejected with 0.2-52% and isolated in high purity. To investigate the catalysts activity after the filtration steps, fresh substrates were added to the solution and the 0.0 Process Step reaction was performed again. The catalyst was still fully active (up to 99%) yield) after batch IV and could be easily reused after the nanofiltration Figure 4. Concentration of the product in the filtration cross flow cell during different reaction batches steps. For all experiments the same membrane (DM 300) was used and shows a good long-term stability with 44 filtration steps. standard.



and diafiltration steps (11 diafiltration steps after each batch). I-IV denote the reaction batches. <sup>a</sup>Determined by GC/MS measurements. <sup>b</sup>Determined by <sup>31</sup>P-NMR measurements with an internal

## Conclusion

With this study we illustrate OSN as an eco-friendly alternative separation without further purification steps. At the same time the catalyst was technology to existing methods for product and catalyst separation. The reused without any loss of activity. Furthermore bifunctional membrane screenings show high rejection rates (>99.1%) for the catalyst. phosphonium salts were synthesized and used as organocatalysts for With the separation experiments we isolated the product in high purity the synthesis of cyclic carbonates from  $CO_2$  and epoxides.

<sup>a</sup> Institute of Chemistry | University of Rostock | Albert-Einstein-Str. 3a | 18059 Rostock | Germany <sup>b</sup> Leibniz Institute for Catalysis | Albert-Einstein-Str. 29 a | 18059 Rostock | Germany

References: [1] a) H. Büttner, K. Lau, A. Spannenberg, T. Werner, ChemCatChem 2015, 7, 459–467. b) T. Werner, H. Büttner, *ChemSusChem* 2014, 7, 3268-3271. [2] T. Fahrenwaldt, J. Großeheilmann, F. Erben, U. Kragl, Org. Process Res. Dev. 2013, 17(9): 1131-1136.

